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T.E. - Sem-I (DBSGS)
Q.P. Code: 574002
Moss Transfer Operations-I
(3 Hours)
[Total Marks: 80]

- N.B. 1) Question No I is compulsory.
 - 2) Attempt any three questions from the remaining five questions.
 - 3) Assume suitable data wherever necessary.
 - 4) Figures to the right indicates full marks.
- . www.a2zsubjects.com
- a) Define molar flux with respect to molar average velocity as well as molar flux with respect to fixed co-ordinates and find relation between them.
 b) Compare penetration theory with surface renewal theory for mass
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transfer coefficient.
c) List advantages of packed bed over tray towers.

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- d) Define Lewis relation. Explain difference between wet bulb temperature and Adiabatic saturation temperature.
 - n 10
- 2. a) Methane diffuses at steady state through a tube containing Helium between two points 0.03m apart. The partial pressures of methane are 55kPa and 15 kPa, when total pressure is 1 atmosphere. If diffusivity is 6.75x10⁻⁵m²/s, and temperature 25°C calculate flux under equimolar counter diffusion and profile of partial pressures between the two points as a function of distance from first point.
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- b) The diffusivity of the gas pair O₂-CCl₄ is determined by observing steady state evaporation of CCl₄ liquid into a tube containing O₂. The entire system is held at constant temperature and pressure. Both the gases are assumed to be ideal and O₂ is stationary. The distance between the CCl₄ liquid level and top of the tube is 0.171m. The total pressure on the system is 100.658x 10³ N/m² and the temperature is 273°K. The vapour pressure of CCl₄ is 4.399x10³N/m² at that temperature. The cross section area of the tube is 0.09x 10⁻³m². After steady state is attained 0.0208x 10⁻⁶m³ of CCl₄ liquid is evaporated in 36000 seconds. What is the diffusivity of gas pairCCL₄-O₂? Assume specific gravity of liquid CCl₄ as 1.59.

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(TURN OVER)

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- 3. a) Describe flux equations for diffusion through polymer membrane and porous 10 solids.
 - b) Explain concept of individual and overall mass transfer coefficient and 10 procedure to calculate interfacial coefficient both graphically and using appropriate formula.
- 4. a) Explain loading and flooding in packed column.

b) 4500kg/hr of SO₂-air mixture containing 5% by volume SO₂ is to be scrubbed with 200,000kg/hr of water in a packed tower. The exit concentration of SO₂ is reduced to 0.15%. The tower operates at one atmosphere. The equilibrium relationship is given by

Y = 30X

Where, Y=Mole SO₂/Mole air

X= Mole SO₂/Mole water

If the packed height of tower is 400cm, estimate the height of transfer unit (H.T.U.).

5. a) A batch of solid for which the following table of data applies is to be 12 dried from 25% to 6% moisture under conditions identical to those for which the data were tabulated. The initial weight of the wet solid is 300kg and the drying surface is 1m²/8kg dry weight. Determine the time for drying.

X	0.35	0.25	0.20	0.13	0.16	0.14	0.12	0.10	0.09	0.08	0.064
N		0.35		0.3	0.26	0.239	0.20	0.18	0.15	0.097	0.07

Where, X=kg moisture/kg dry solid

N=kg moisture evaporated/hr m²

b) Explain the mechanism of batch drying.

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6. Write short notes on any four:

- a) Wetted wall column
- b) Mass transfer analogy
- c) Overall tray efficiency
- d) Natural draft and forced draft cooling towers
- e) Humid heat and humid volume

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